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## Computer Program for Lithium Hydroxide — Carbon Dioxide Absorption in Underwater Life Support Systems

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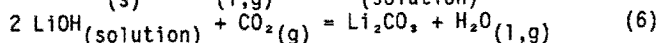
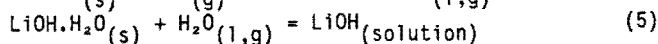
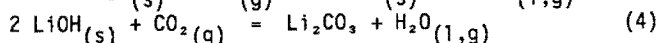
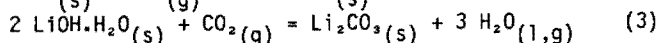
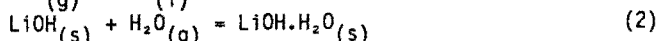
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### ABSTRACT

Lithium hydroxide (LiOH) has been used as a CO<sub>2</sub> absorbent in underwater life support systems and the space industry. The effectiveness of the LiOH-CO<sub>2</sub> reaction is a function of temperature, humidity, composition of incoming gas, method of packing, geometry of canister, granular size and porosity of the absorbent. Laboratory tests are performed to determine the effects of these factors on LiOH bed-CO<sub>2</sub> absorption. The resulting information can be used to establish an analytical model for LiOH absorber design analysis in underwater life support systems. A computer program is presented to design a LiOH absorber in a manned submersible.

### INTRODUCTION

Lithium hydroxide has been used as an absorbent to remove carbon dioxide in an enclosed space (1,2,3). Over the years, a considerable number of studies (4,5,6,7,8) were conducted to improve carbon dioxide removal with the use of lithium hydroxide. As lithium hydroxide absorbs carbon dioxide from a gas stream, the chemical reactions between LiOH and CO<sub>2</sub> can be expressed as:



The effectiveness of the LiOH-CO<sub>2</sub> reaction varies with temperature, humidity, composition of incoming gas, method of packing, geometry of canister, granular size and porosity of the absorbent (9,10,11,12,13). The hydration of LiOH to monohydrate lithium hydroxide is

the initial step toward reaction between CO<sub>2</sub> and LiOH. If an insufficient amount of water vapor in the air stream exists, then the small amount of monohydrate lithium hydroxide formed will allow only partial reaction with carbon dioxide. On the other hand, an excessive quantity of water vapor forms a saturated LiOH·H<sub>2</sub>O solution. Water film around the LiOH granules hinders the reaction and results in an incomplete absorption between LiOH and CO<sub>2</sub> (9,13). Therefore, a suitable amount of water vapor, which is regulated by temperature and/or relative humidity, is one of the determining factors to achieve an optimal use of LiOH to remove CO<sub>2</sub>.

In addition to the water content, other factors such as CO<sub>2</sub> concentration in the gas stream and residence time also control the absorption efficiency of LiOH. A short residence time normally causes an incomplete chemical reaction and the CO<sub>2</sub> absorption capacity of the absorbent is decreased. However, a longer residence time requires a lower scrubbing rate through the scrubber. This results in CO<sub>2</sub> accumulation in the enclosed space when the CO<sub>2</sub> scrubbing rate is lower than the CO<sub>2</sub> production rate. The optimal residence time and scrubbing rate are needed in order to maintain a desirable CO<sub>2</sub> concentration in the enclosed space (8).

Residence time is defined as the time required for a specific volume of gas to travel through the interstitial spaces within the LiOH canister. Scrubbing rate and the volume available for gas flow control residence time. The available volume in the canister is determined by the granular size, weight of granules and method of packing. For the same amount of absorbent, particles with a smaller granular size have a tendency to be packed more densely than those with a larger granular size. Therefore, residence time of the CO<sub>2</sub> molecule in the canister would vary with granular size.

APPARATUS AND PROCEDURE

A series of laboratory tests were conducted to investigate the effects of environmental and geometric parameters on CO<sub>2</sub> absorption. The parameters studied include the gas flow rate, gas temperature, humidity, scrubber length and diameter, granular size and CO<sub>2</sub> concentration. Figure 1 shows laboratory equipment set-up for this study.

Each experiment was terminated when the exit air stream from the absorbent tube reached 0.51% CO<sub>2</sub>. The time when experiments began until 0.51% CO<sub>2</sub> reached in the exit gas is defined as the breakthrough time (t<sub>B</sub>). The ratio of breakthrough time (t<sub>B</sub>) to theoretical time (t<sub>TH</sub>) is the efficiency of LiOH absorption capacity. Theoretical time is the time required when the amount of LiOH completely reacted with CO<sub>2</sub>. Theoretical time can be expressed as:

$$t_{(TH)} = \frac{1}{2} \left( \frac{W_a}{M_{LiOH}} \right) \left( \frac{R_g T}{P_T} \right) \left( \frac{1}{V_f C_{in}} \right) \quad (7)$$

Plots of efficiency vs. flow rate or residence time were used to illustrate the effects of different parameters on the CO<sub>2</sub> absorption (14).

RESULTS AND DISCUSSION

Temperature effects were studied at 40, 26.5, 15 and 5°C with the gas stream at relative humidity greater than 85%. The results are shown in Figure 2. Because the partial pressure of water vapor decreased with temperature decreased, the lower temperature required a longer residence time to achieve the same efficiency as the higher temperature. The optimal residence times were 0.21, 0.34, 0.55 and 2.55 sec. at 40, 26.5, 15 and 5°C, respectively, for each experimental run. The results indicate the optimal residence time increased as temperature decreased.

Figure 3 displays the humidity effects on the CO<sub>2</sub> absorption. When humidity was less than 70%, the optimal residence time was greater than 0.7 seconds. However, the optimal residence time for a gas stream with humidity greater than 70% was found to be only 0.34 seconds. This shows that lower humidity in the gas stream requires longer residence time in order to have higher absorption efficiency. Figure 4 illustrates the residence time effect on length-to-diameter ratios (L/D) for an axial canister. The results show (L/D) ratio had little effect on CO<sub>2</sub> absorption at the same residence time. The effect of LiOH granular size on the absorption efficiency is shown in Figure 5. Two and one half grams of LiOH with different granular sizes of 0.62, 0.47, and 0.32 cm packed in a 1 cm i.d. reaction tube resulted in a bed length of 8.1, 7.1 and 6.5 cm, respectively. Figure 5 shows when residence time was greater than 0.6 seconds, smaller granular size had less efficiency. The CO<sub>2</sub> concentration in the inlet gas stream also affected absorption efficiency. Concentrations of 1.0%, 2.4% and 4.8% CO<sub>2</sub> in the gas stream were studied. Figure 6 that shows when residence time was less than 0.5 seconds, a lower CO<sub>2</sub> concentration had higher absorption efficiency. Because the shorter residence time resulted in higher flow rate, the lower CO<sub>2</sub> concentration had a more complete reaction with LiOH than with the higher

concentrations. Based on the resulting absorption characteristic for each factor controlling the LiOH-CO<sub>2</sub> reaction, an analytical model was established to predict the effectiveness of LiOH absorber in underwater life support systems (15).

COMPUTER PROGRAM FOR DETERMINING ABSORBER'S VOLUME AND EQUILIBRIUM SCRUBBING RATE

The empirical data of the LiOH-CO<sub>2</sub> reaction obtained from this study was programmed to determine the absorber's volume and equilibrium scrubbing rate. The flowchart and input parameters have been shown in Tables 1 and 2, respectively. The absorption efficiency of 1% CO<sub>2</sub> of incoming gas stream at 26.5 °C and R.H. greater 85% (saturated) was used as the standard absorption efficiency. Temperature, humidity and CO<sub>2</sub> concentration correlative factors were obtained from subroutine "TEMP", "HUMID" and "CONC", respectively. The overall efficiency, scrubber volume, scrubbing rate and residence time were computed in the main program (see Appendix). A sample illustration using the program to determine the parameters of an absorber is presented. The absorber is to be operated at 26.5°C and 1 atm. for 5 hours with two divers in a manned submersible (volume = 3.14 m<sup>3</sup> and relative humidity > 85%):

```

ENVIRONMENTAL CONDITIONS
TEMPERATURE AT 5, 15, 26.5 OR 40 C; INPUT IT
IF TEMP = 5.0 C, IT = 1 (TYPE 1)
IF TEMP = 15.0 C, IT = 2 (TYPE 2)
IF TEMP = 26.5 C, IT = 3 (TYPE 3)
IF TEMP = 40.0 C, IT = 4 (TYPE 4)
3<CR>
HUMIDITY OF < 10, 30-40, 60-70 OR > 85%; INPUT IH
IF HUMID < 10% (DRY), IH = 1 (TYPE 1)
IF HUMID = 30-40%, IH = 2 (TYPE 2)
IF HUMID = 60-70%, IH = 3 (TYPE 3)
IF HUMID > 85% (SATURATED), IH = 4 (TYPE 4)
4<CR>
ENTER PARTIAL PRESSURE OF CO2, ATM
IF CONC = 1.0%, TYPE 0.01
IF CONC = 2.4%, TYPE 0.024
IF CONC = 4.8%, TYPE 0.048
0.01<CR>
PRESSURE, ATM
1<CR>
HOW MANY PERSONS ARE IN THE CHAMBER?
2<CR>
HOW MANY HOURS ARE REQUIRED?
5<CR>
CO2 PRODUCTION RATE, GRAM/HOUR/PERSON
52<CR>
RATIO OF SCRUBBER LENGTH TO DIAMETER
3.6<CR>

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ENVIRONMENTAL CONDITIONS
TEMPERATURE = 26.5000 C
PRESSURE = 1.00000 ATM
MAX. ALLOWABLE CO2 MOLAR FRACTION = 1.000000E-02
HUMIDITY > 85% (SATURATED)
PERSON = 2.00000
TIME = 5.00000 HOUR

DESIGN CRITERIA
NO. OF ITERATION = 1
SCRUBBER VOLUME = 1614.00 CC
LENGTH = 29.8647 CM
DIAMETER = 8.29522 CM
VELOCITY = 29.8543 CM/SEC

```

AMOUNT OF LIOH PACKED = 743.410 G  
 SCRUBBER FLOW RATE = 1613.44 CC/SEC  
 RESIDENCE TIME (LAST-1) = 0.653870 SEC  
 RESIDENCE TIME (LAST) = 0.650226 SEC  
 OVERALL EFFICIENCY = 0.760303

END OF COMPUTATION  
 \*\*\*\*STOP

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APPENDIX

```

PROGRAM SCRUBBER
REAL PERSON,HOUR,T,P,CO2,RTNEW,RCO2,LENGTH
INTEGER IT,IH,IC
OPEN (UNIT=6,FILE='TAEM',STATUS='NEW')
OPEN (UNIT=7,FILE='SOUT',STATUS='NEW')
*****INPUT DATA INTERACTIVELY
WRITE (1,*) 'ENVIRONMENTAL CONDITIONS'
WRITE (1,*) 'TEMPERATURE AT 5, 15, 26.5 OR 40 C;
INPUT IT'
WRITE (1,*) 'IF TEMP = 5.0 C, IT = 1 (TYPE 1)'
WRITE (1,*) 'IF TEMP = 15.0 C, IT = 2 (TYPE 2)'
WRITE (1,*) 'IF TEMP = 26.5 C, IT = 3 (TYPE 3)'
WRITE (1,*) 'IF TEMP = 40.0 C, IT = 4 (TYPE 4)'
READ (1,*) IT
IF (IT .EQ. 1) T = 5.0
IF (IT .EQ. 2) T = 15.0
IF (IT .EQ. 3) T = 26.5
IF (IT .EQ. 4) T = 40.0
WRITE (1,*) 'HUMIDITY OF < 10, 30-40, 60-70 OR >
85%; INPUT IH'
WRITE (1,*) 'IF HUMID < 10% (DRY),          IH = 1
(TYPE 1)'
WRITE (1,*) 'IF HUMID = 30-40%,          IH = 2
(TYPE 2)'
WRITE (1,*) 'IF HUMID = 60-70%,          IH = 3
(TYPE 3)'
WRITE (1,*) 'IF HUMID > 85% (SATURATED), IH = 4
(TYPE 4)'
READ (1,*) IH
WRITE (1,*) 'ENTER PARTIAL PRESSURE OF CO2, ATM'
WRITE (1,*) 'IF CONC = 1.0%, TYPE 0.01'
WRITE (1,*) 'IF CONC = 2.4%, TYPE 0.024'
WRITE (1,*) 'IF CONC = 4.8%, TYPE 0.048'
READ (1,*) CO2
IF (CO2 .LE. 0.017) IC = 1
IF ((CO2 .GT. 0.017) .AND. (CO2 .LE. 0.036)) IC
= 2
IF (CO2 .GT. 0.036) IC = 3
WRITE (1,*) 'PRESSURE, ATM'
READ (1,*) P
WRITE (1,*) 'HOW MANY PERSONS ARE IN THE
CHAMBER?'
READ (1,*) PERSON
WRITE (1,*) 'HOW MANY HOURS ARE REQUIRED?'
READ (1,*) HOUR
WRITE (1,*) 'CO2 PRODUCTION RATE,
GRAM/HOUR/PERSON'
WRITE (1,*) 'FOR NORMAL CONDITION, SUGGESTED
VALUE = 52'

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READ (1,*) RCO2
WRITE (1,*) 'RATIO OF SCRUBBER LENGTH TO
DIAMETER'
READ (1,*) RLD
WRITE (1,*) 'TO ENTER DESIRED LENGTH AND
DIAMETER, TYPE 1'
WRITE (1,*) 'OR TYPE 2 FOR COMPUTER GENERATED
VALUES'
READ (1,*) ILD
IF (ILD .EQ. 2) GO TO 5
WRITE (1,*) 'INPUT DIAMETER AND LENGTH (CM)'
READ (1,*) D,LENGTH
5 WRITE (1,*) 'VOLUMETRIC FLOW RATE, CM/SEC'
READ (1,*) VF
WRITE (1,*) 'TO ENTER GRAMS LIOH PACKED, TYPE 1'
WRITE (1,*) 'OR TYPE 2 FOR COMPUTER GENERATED
VALUES'
READ (1,*) IG
IF (IG .EQ. 2) GO TO 6
WRITE (1,*) 'ENTER LIOH PACKED (GRAM)'
READ (1,*) TOTLIOH
6 RTO = 0.19
*****INITIALIZATION
IRT = 0
SAFE = 0.85
VOID = 0.65
DLIOH = 1.316
DCO2 = P/0.08205/(T+273)*44.0
*****BEGINNING OF A NEW RESIDENCE TIME
10 RTO = RTO + 0.01
RTNEW = RTO
IRT = IRT + 1
ICOUNT = 0
*****ITERATION
20 RT = RTNEW
ICOUNT = ICOUNT + 1
*****STANDARD EFFICIENCY AT 26.5 C, R.H. 85%, 1% OF
CO2
IF (RT .LT. 0.182) GO TO 11
IF ((RT .GE. 0.182) .AND. (RT .LT. 0.198)) GO TO
12
IF ((RT .GE. 0.198) .AND. (RT .LT. 0.219)) GO TO
13
IF ((RT .GE. 0.219) .AND. (RT .LT. 0.282)) GO TO
14
IF ((RT .GE. 0.282) .AND. (RT .LT. 0.336)) GO TO
15
IF ((RT .GE. 0.336) .AND. (RT .LT. 0.522)) GO TO
16
IF ((RT .GE. 0.522) .AND. (RT .LT. 1.088)) GO TO
17
IF ((RT .GE. 1.088) .AND. (RT .LT. 3.161)) GO TO
18
EFF = 0.573
GO TO 100
11 EFF = 0.123
GO TO 100
12 EFF = 0.123 + 1.5625000*(RT-0.182)
GO TO 100
13 EFF = 0.148 +26.7619040*(RT-0.198)
GO TO 100
14 EFF = 0.710 + 2.0793650*(RT-0.219)
GO TO 100
15 EFF = 0.841 + 1.0000000*(RT-0.282)
GO TO 100
16 EFF = 0.895 - 0.5913978*(RT-0.336)
GO TO 100
17 EFF = 0.785 - 0.1872791*(RT-0.522)
GO TO 100
18 EFF = 0.679 - 0.0511336*(RT-1.088)
100 EFFSTD = EFF
*****CALL SUBROUTINE HUMID, TEMP, CONC
CALL HUMID (IH,EFFSTD,RT,EFFH)

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CALL TEMP (IT,EFFSTD,RT,EFFT)
CALL CONC (IC,EFFSTD,RT,EFFC)
*****OVERALL EFFICIENCY
EFFFALL = EFFH*EFFT*EFFC*EFFSTD
IF (EFFFALL .GT. 1.E-10) GO TO 150
WRITE(1,*) 'OVERALL EFFICIENCY = 0'
GO TO 200
*****COMPUTE MINIMUM CANISTER VOLUME
150 TOTCO2 = RCO2*PERSON*HOUR
IF (IG .EQ. 1) GO TO 155
TOTLIOH = TOTCO2/0.92/EFFFALL
155 IF (ILD .EQ. 1) GO TO 160
VOL = TOTLIOH/DLIOH/(1.0-VOID)
GO TO 170
160 VOL = 3.1416*D*D/4.*LENGTHH
*****COMPUTE SCRUBBER FLOW RATE
* VF = RCO2*PERSON/(CO2*SAFE -0.005)/DCO2*1000.
/3600.
*****COMPUTE NEW RESIDENCE TIME FROM CANISTER VOLUME
AND FLOW RATE
170 RTNEW = VOL*VOID/VF
*****IF NO OF ITERATIONS > 5, STOP
IF (ICOUNT .GT. 5) GO TO 200
*****IF DIFFERENCE BETWEEN NEW AND OLD RESIDENCE TIME
< 1% OF OLD
*****RESIDENCE TIME, STOP; OTHERWISE, CONTINUE
DIFF = ABS (RTNEW - RT)
CHECK = DIFF/RT
IF (DIFF .GT. 0.01) GO TO 20
*****IF IT CAN'T BE CONVERGED WITHIN 5 TRIALS, THEN
TRY A NEW GUESS RT
*****BY INCREMENT OF 0.01 SEC
200 IF ((IRT .LT. 180) .AND. (ICOUNT .GT. 5)) GO TO
10
*****COMPUTE SCRUBBER LENGTH, DIAMETER AND VELOCITY
IF (ILD .EQ. 1) GO TO 210
D = (VOL*4.0/RLD/3.1416)**(0.33333)
LENGTH = VOL*4.0/3.1416/D/D
210 U = VF*4.0/3.1416/D/D
*****PRINT THE FINAL RESULTS
WRITE (1,*) ' ENVIRONMENTAL CONDITIONS'
WRITE (1,*) ' TEMPERATURE = ',T,' C'
WRITE (1,*) ' PRESSURE = ',P,' ATM'
WRITE (1,*) ' MAX. ALLOWABLE CO2 MOLAR FRACTION
= ',CO2
WRITE (7,*) ' ENVIRONMENTAL CONDITIONS'
WRITE (7,*) ' TEMPERATURE = ',T,' C'
WRITE (7,*) ' PRESSURE = ',P,' ATM'
WRITE (7,*) ' MAX. ALLOWABLE CO2 MOLAR FRACTION
= ',CO2
IF (IH .NE. 1) GO TO 240
WRITE (1,*) ' HUMIDITY < 10% (DRY)'
WRITE (7,*) ' HUMIDITY < 10% (DRY)'
GO TO 270
240 IF (IH .NE. 2) GO TO 250
WRITE (1,*) ' HUMIDITY = 30-40%'
WRITE (7,*) ' HUMIDITY = 30-40%'
GO TO 270
250 IF (IH .NE. 3) GO TO 260
WRITE (1,*) ' HUMIDITY = 60-70%'
WRITE (7,*) ' HUMIDITY = 60-70%'
GO TO 270
260 WRITE (1,*) ' HUMIDITY > 85% (SATURATED)'
WRITE (7,*) ' HUMIDITY > 85% (SATURATED)'
270 WRITE (1,*) ' PERSON = ',PERSON
WRITE (1,*) ' TIME = ',HOUR,' HOUR'
WRITE (1,275)
WRITE (1,*) ' DESIGN CRITERIA'
WRITE (1,*) ' NO. OF ITERATION = ',IRT
WRITE (1,300) VOL,LENGTH,D,U
WRITE (1,350) TOTLIOH,VF,RT,RTNEW,EFFFALL
275 FORMAT (/)

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300 FORMAT (2X,'SCRUBBER VOLUME = ',G12.6,'
      CC',/,2X,'LENGTH = ',
1 G12.6,' CM',/,2X,'DIAMETER = ',G12.6,'
      CM',/,2X,'VELOCITY = ',
2 G12.6,' CM/SEC')
350 FORMAT (2X,'AMOUNT OF LIQH PACKED = ',G12.6,'
      G',/,2X,
2 'SCRUBBER FLOW RATE = ',G12.6,'CC/SEC',/,2X,'
      RESIDENCE TIME (LAS
3T-1) = ',G12.6,' SEC',/,2X,'RESIDENCE TIME
      (LAST) = ',G12.6,
4 ' SEC',/,2X,'OVERALL EFFICIENCY = ',G12.6)
WRITE (7,*) 'PERSON = ',PERSON
WRITE (7,*) 'TIME = ',HOUR,' HOUR'
WRITE (7,275)
WRITE (7,*) 'DESIGN CRITERIA'
WRITE (7,*) 'NO. OF ITERATION = ',IRT
WRITE (7,300) VOL,LENGTH,D,U
WRITE (7,350) TOTLIQH,VF,RT,RTNEW,EFFALL
WRITE (1,275)
WRITE (1,*) 'END OF COMPUTATION'
WRITE (6,*) LENGTH,U,D,VF
WRITE (6,*) TOTLIQH,P,HOUR,PERSON,RCO2
WRITE (6,*) IC,IH,IT
STOP
END
*****
****SUBROUTINE HUMIDITY
SUBROUTINE HUMID (IH,EFFSTD,RT,EFFH)
IF (IH .EQ. 1) GO TO 10
IF (IH .EQ. 2) GO TO 20
IF (IH .EQ. 3) GO TO 30
IF (IH .EQ. 4) GO TO 40
****HUMIDITY LESS THAN 10%
10 IF (RT .LT. 0.169) GO TO 11
IF ((RT .GE. 0.169) .AND. (RT .LT. 0.335)) GO TO
12
IF ((RT .GE. 0.335) .AND. (RT .LT. 1.027)) GO TO
13
IF ((RT .GE. 1.027) .AND. (RT .LT. 2.992)) GO TO
14
EFF = 1.0
GO TO 100
11 EFF = 0.207
GO TO 100
12 EFF = 0.207 + 2.2771084*(RT-0.169)
GO TO 100
13 EFF = 0.585 + 0.4638728*(RT-0.335)
GO TO 100
14 EFF = 0.906 + 0.0478371*(RT-1.027)
GO TO 100
****HUMIDITY 30-40%
20 IF (RT .LT. 0.160) GO TO 21
IF ((RT .GE. 0.160) .AND. (RT .LT. 0.236)) GO TO
22
IF ((RT .GE. 0.236) .AND. (RT .LT. 0.705)) GO TO
23
IF ((RT .GE. 0.705) .AND. (RT .LT. 1.197)) GO TO
24
EFF = 0.974
GO TO 100
21 EFF = 0.183
GO TO 100
22 EFF = 0.183 + 2.1052631*(RT-0.160)
GO TO 100
23 EFF = 0.343 + 1.2153518*(RT-0.236)
GO TO 100
24 EFF = 0.913 + 0.1239837*(RT-0.705)
GO TO 100
****HUMIDITY 60-70%
30 IF (RT .LT. 0.145) GO TO 31
IF ((RT .GE. 0.145) .AND. (RT .LT. 0.257)) GO TO
32

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IF ((RT .GE. 0.257) .AND. (RT .LT. 0.323)) GO TO
33
IF ((RT .GE. 0.323) .AND. (RT .LT. 0.912)) GO TO
34
EFF = 0.804
GO TO 100
31 EFF = 0.098
GO TO 100
32 EFF = 0.098 + 1.9642857*(RT-0.145)
GO TO 100
33 EFF = 0.318 + 3.5909090*(RT-0.257)
GO TO 100
34 EFF = 0.555 + 0.4227504*(RT-0.323)
GO TO 100
****HUMIDITY GREATER THAN 85%
40 EFF = EFFSTD
****
100 IF (EFF .LT. 1.0E-10) WRITE (1,*) 'EFFICIENCY
      (HUMID) = 0'
EFFH = EFF/EFFSTD
RETURN
END
*****
****SUBROUTINE TEMPERATURE
SUBROUTINE TEMP (IT,EFFSTD,RT,EFFT)
IF (IT .EQ. 1) GO TO 10
IF (IT .EQ. 2) GO TO 20
IF (IT .EQ. 3) GO TO 30
IF (IT .EQ. 4) GO TO 40
****TEMPERATURE AT 5 C
10 IF (RT .LT. 0.164) GO TO 11
IF ((RT .GE. 0.164) .AND. (RT .LT. 0.405)) GO TO
12
IF ((RT .GE. 0.405) .AND. (RT .LT. 0.838)) GO TO
13
IF ((RT .GE. 0.838) .AND. (RT .LT. 2.551)) GO TO
14
EFF = 0.824
GO TO 100
11 EFF = 0.066
GO TO 100
12 EFF = 0.066 + 2.2074688*(RT-0.164)
GO TO 100
13 EFF = 0.598 + 0.4826789*(RT-0.405)
GO TO 100
14 EFF = 0.807 + 0.0099241*(RT-0.838)
GO TO 100
****TEMPERATURE AT 15 C
20 IF (RT .LT. 0.140) GO TO 21
IF ((RT .GE. 0.140) .AND. (RT .LT. 0.364)) GO TO
22
IF ((RT .GE. 0.364) .AND. (RT .LT. 1.035)) GO TO
23
EFF = 0.880
GO TO 100
21 EFF = 0.088
GO TO 100
22 EFF = 0.088 + 3.5848214*(RT-0.140)
GO TO 100
23 EFF = 0.891 - 0.0163934*(RT-0.364)
GO TO 100
****TEMPERATURE AT 26.5 C
30 EFF = EFFSTD
GO TO 100
****TEMPERATURE AT 40 C
40 IF (RT .LT. 0.153) GO TO 41
IF ((RT .GE. 0.153) .AND. (RT .LT. 0.207)) GO TO
42
IF ((RT .GE. 0.207) .AND. (RT .LT. 0.560)) GO TO
43
IF ((RT .GE. 0.560) .AND. (RT .LT. 2.482)) GO TO
44
EFF = 0.354

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GO TO 100
41 EFF = 0.688
GO TO 100
42 EFF = 0.688 + 0.0944444*(RT-0.153)
GO TO 100
43 EFF = 0.739 + 0.6968838*(RT-0.207)
GO TO 100
44 EFF = 0.493 + 0.0732040*(RT-0.560)
*****
100 IF (EFF .LT. 1.0E-10) WRITE (1,*) 'EFFICIENCY
      (TEMP) = 0'
      EFFT = EFF/EFFSTD
      RETURN
      END
*****
*****SUBROUTINE CONCENTRATION
SUBROUTINE CONC (IC,EFFSTD,RT,EFFC)
IF (IC .EQ. 1) GO TO 10
IF (IC .EQ. 2) GO TO 20
IF (IC .EQ. 3) GO TO 30
*****CONCENTRATION OF 1%
10 EFF = EFFSTD
GO TO 100
*****CONCENTRATION OF 2.4%
20 IF (RT .LT. 0.169) GO TO 21
   IF ((RT .GE. 0.169) .AND. (RT .LT. 0.299)) GO TO
   22
   IF ((RT .GE. 0.299) .AND. (RT .LT. 0.553)) GO TO
   23
   IF ((RT .GE. 0.553) .AND. (RT .LT. 0.856)) GO TO
   24
   IF ((RT .GE. 0.856) .AND. (RT .LT. 3.154)) GO TO
   25
   EFF = 0.739
   GO TO 100
21 EFF = 0.088
GO TO 100
22 EFF = 0.088 + 0.2615384*(RT-0.169)
GO TO 100
23 EFF = 0.122 + 1.3661417*(RT-0.299)
GO TO 100
24 EFF = 0.469 + 0.6633663*(RT-0.553)
GO TO 100
25 EFF = 0.670 + 0.0300261*(RT-0.856)
GO TO 100
*****CONCENTRATION OF 4.8%
30 IF (RT .LT. 0.169) GO TO 31
   IF ((RT .GE. 0.169) .AND. (RT .LT. 1.698)) GO TO
   32
   IF ((RT .GE. 1.698) .AND. (RT .LT. 3.123)) GO TO
   33
   EFF = 0.783
   GO TO 100
31 EFF = 0.097
GO TO 100
32 EFF = 0.097 + 0.3629823*(RT-0.169)
GO TO 100
33 EFF = 0.652 + 0.0919298*(RT-1.698)
*****
100 IF (EFF .LT. 1.0E-10) WRITE (1,*) 'EFFICIENCY
      (CONE) = 0'
      EFFC = EFF/EFFSTD
      RETURN
      END

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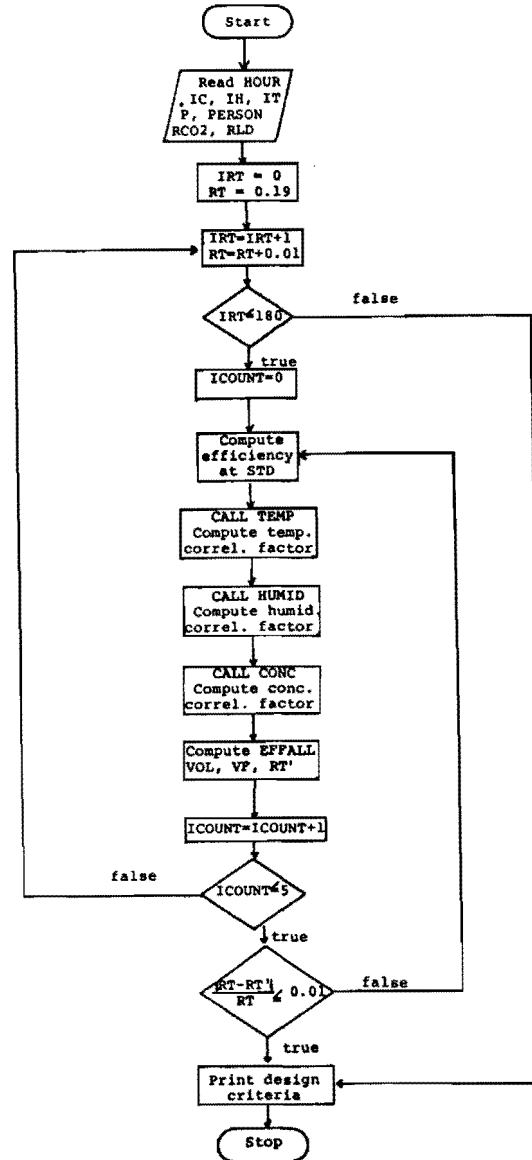


Table 1. Flowchart "Scrubber"

Table 2. Input Parameters of "SCRUBBER" Program.

Parameter	Description	
CO2	partial pressure of CO <sub>2</sub> , atm	
HOURL	duration period, hour	
IH	relative humidity	
	if humidity < 10% (dry),	IH = 1
	if humidity = 30-40%,	IH = 2
	if humidity = 60-70%,	IH = 3
if humidity > 85%	IH = 4	
IT	temperature	
	if temperature = 5.0 °C,	IT = 1
	if temperature = 15.0 °C,	IT = 2
	if temperature = 26.5 °C,	IT = 3
if temperature = 40.0 °C,	IT = 4	
P	pressure, atm	
PERSON	number of people in the chamber	
ROO2	CO <sub>2</sub> production rate, gram of ROO2 = 52, for normal condition	
RLD	ratio of scrubber length to diameter	

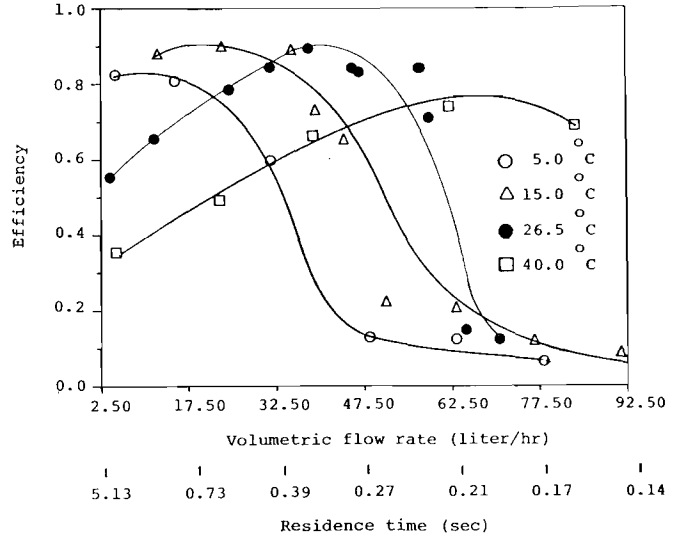


Figure 2. The effects of temperature on LiOH-CO<sub>2</sub> absorption.

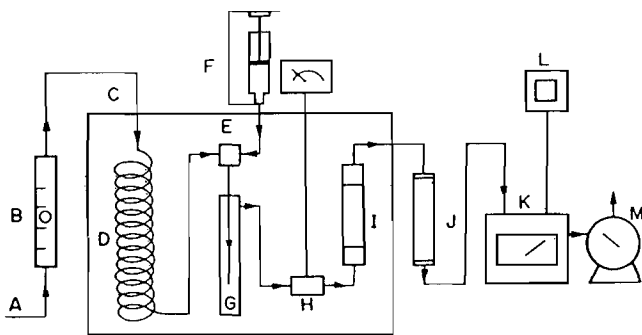


Figure 1. Dynamic gas flow system. A: Inlet air stream; B: Flow meter; C: Temperature controlled water bath; D: Copper coil, 20 ft x 1/8 in; E: Air-water mixer; F: Syringe pump; G: Midget bubbler; H: Temperature and humidity sensor; I: Absorbent tube; J: Drying tube; K: CO<sub>2</sub> detector; L: Strip chart recorder; M: Wet test meter.

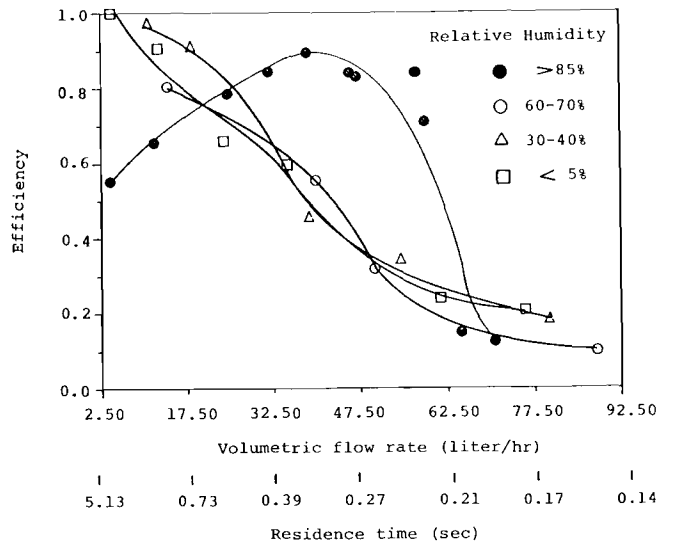


Figure 3. The effects of humidity on the LiOH-CO<sub>2</sub> absorption.



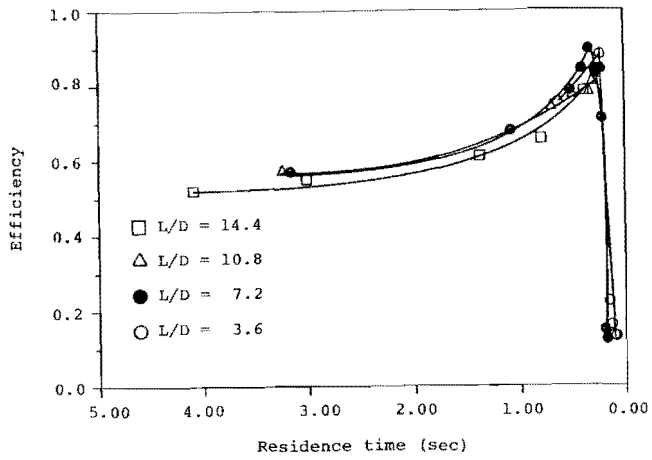


Figure 4. The effects of (L/D) ratio on the LiOH-CO<sub>2</sub> absorption.

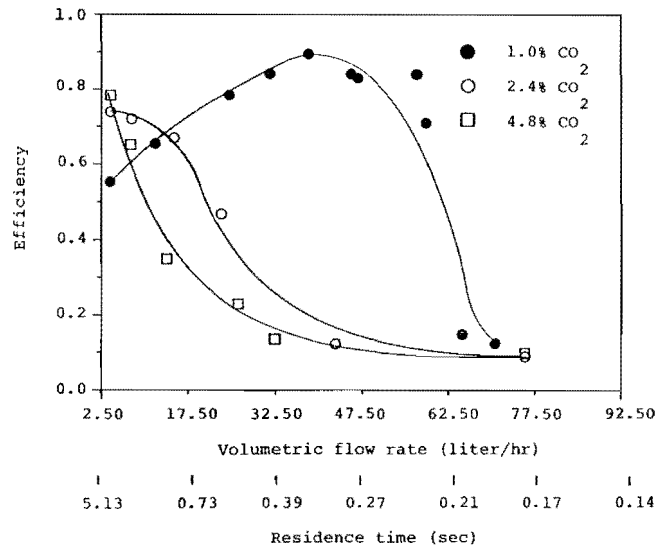


Figure 6. The effects of CO<sub>2</sub> concentration on the LiOH-CO<sub>2</sub> absorption.

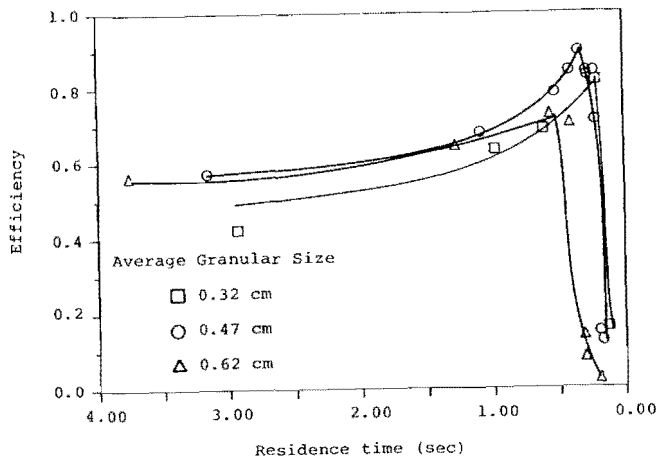


Figure 5. The effects of granular size on the LiOH-CO<sub>2</sub> absorption.